

# A Non-Newtonian rheology model application to complex flows (PyroClast)

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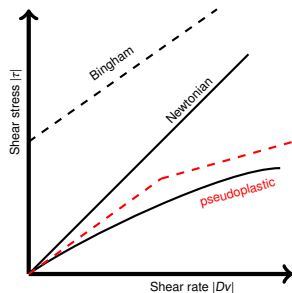
CEMRACS 2019  
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- Motivation
- Newtonian fluid (**Known model**)
  - Lubrication approximation
  - Lubrication model
  - Numerical results
- Bingham fluid (**Known model**)
  - Navier-Stokes model for Bingham fluid
  - Lubrication model
  - Numerical results
- Two viscosities model (**New model**)
  - Two-viscosities model for pseudo-viscoplastic fluid
  - Lubrication model
  - Numerical results

# Motivation



Pyroclast flow (Source: Internet)



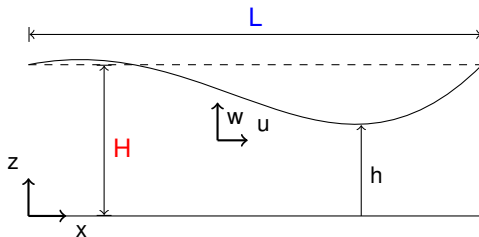
Rheology - types

**Idea:** To approximate the pseudo-plastic rheology by a piecewise affine function.

# Main features

- $H/L \ll 1$  Lubrication approximation
- Rheology - type (Stress-Strain relation).
  - Newtonian fluid : Water, oil,....
  - Bingham fluid
  - Two - viscosities model: "Pseudo-viscoplastic fluid"

## Navier-Stokes model



## Navier-Stokes model

$$u_x + w_z = 0$$

$$\rho(u_t + uu_x + ww_z) = -p_x + 2\mu u_{xx} + \mu u_{zz} + \mu w_{xz}$$

$$\rho(w_t + uw_x + ww_z) = -p_z + \mu u_{xz} + \mu w_{zz} + 2\mu w_{zz} - \rho g$$

## Boundary condition

$$u = w = 0$$

$$z = 0$$

$$(1 - h_x^2)p + 2\mu(1 + h_x)^2 u_x = 0 \quad z = h(x, t)$$

$$(1 - h_x^2)(u_z + w_x) - 4h_x u_x = 0 \quad z = h(x, t)$$

## Kinematic condition

$$h_t + uh_x = w \quad z = h(x, t)$$

## Scale independent

$$x = L\tilde{x}, \quad z = H\tilde{z}, \quad u = U\tilde{u}$$

## Scale dependent

$$h = H\tilde{h}, \quad t = \frac{L}{U}\tilde{t}, \quad w = \frac{H}{LU}\tilde{w}, \quad p = \rho g H\tilde{p}$$

$$\varepsilon = \frac{H}{L}, \quad Fr^2 = \frac{U^2}{gH}, \quad Re = \frac{\rho HU}{\mu}$$

## Dimensionless equation

$$\varepsilon Re(u_t + uu_x + wu_z) = -\frac{\varepsilon Re}{Fr^2} p_x + 2\varepsilon^2 \mu u_{xx} + u_{zz} + \varepsilon^2 w_{xz}$$

$$\varepsilon^3 Re(w_t + uw_x + ww_z) = -\frac{\varepsilon Re}{Fr^2} p_z + \varepsilon^4 \mu w_{xx} + \varepsilon^2 u_{xz} + 2\varepsilon^2 w_{zz} - 1$$

## Limit problem

$$u_x + w_z = 0, \quad p_x = u_{zz}, \quad p_z = -1$$

## Boundary condition

$$u = w = 0 \quad z = 0$$

$$p = u_z = 0 \quad z = h(x, t)$$

## Kinematic condition

$$h_t + uh_x = w \quad z = h(x, t)$$

## Lubrication model

$$h_t - \partial_x \left( \frac{h^3}{3} h_x \right) = 0$$

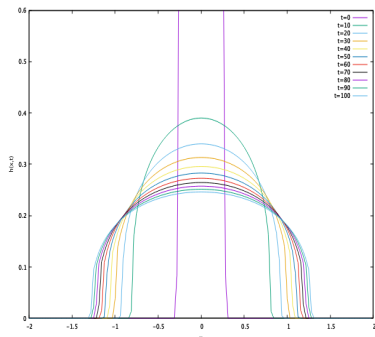
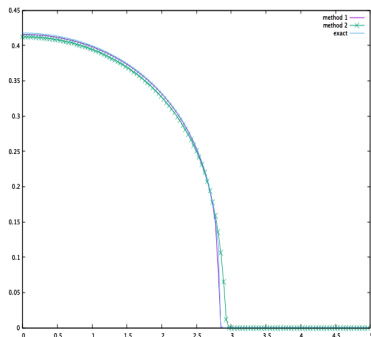
# Numerical results

- Method 1:

$$F(H_l, H_r) = -\left(\frac{H_L + H_R}{2}\right)^3 \frac{H_R - H_L}{3\Delta x}$$

- Method 2:

$$F(H_l, H_r) = \frac{(H_L - H_R)(H_L^3 + H_R^3)}{6\Delta x} - \frac{|H_L - H_R| \max(H_L^2, H_R^2)(H_R - H_L)}{2\Delta x}$$





# Bingham fluid

- $v = (u, w)^T$
- $Dv = \frac{\nabla v + \nabla v^T}{2}$ ,  $\tau = \begin{pmatrix} \tau_{xx} & \tau_{xz} \\ \tau_{xz} & \tau_{zz} \end{pmatrix}$

## Laws of behavior

### Newtonian fluid

$$\tau = 2\mu Dv$$

### Bingham fluid

$$\begin{cases} |\tau| < Bi & Dv = 0 \quad \text{solid} \\ \tau = Dv + Bi \frac{Dv}{|Dv|} & Dv \neq 0 \quad \text{fluid} \end{cases}$$

## Limit problem

### Newtonian fluid

$$p_x = u_{zz}$$

### Bingham fluid

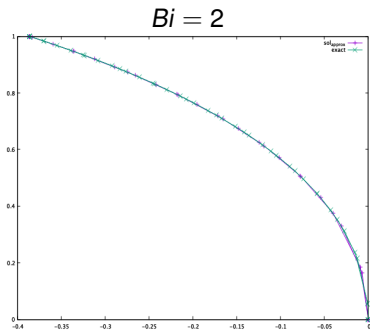
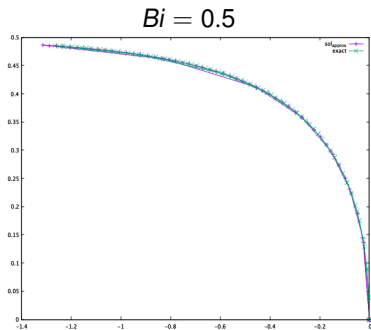
$$p_x = 2\partial_z \tau_{xz} = \partial_z \left( u_z \left( 1 + \frac{Bi \sqrt{2}}{|u_z|} \right) \right)$$

# Lubrication model - Numerical results

$$h_t - \partial_x \left( \frac{h_x Y^2}{6} [3h - Y] \right) = 0$$

$$Y = \max \left( h - \frac{Bi \sqrt{2}}{|h_x|}, 0 \right)$$

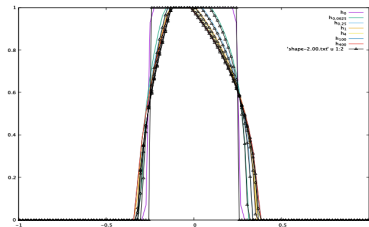
**Remark:**  $Bi = 0$  Bingham  $\rightarrow$  Newtonian



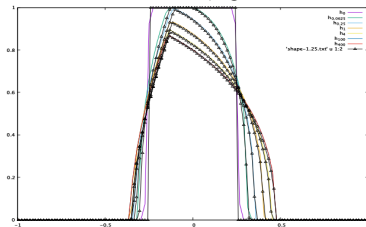
$nx = 128$

# Numerical results - Slump test

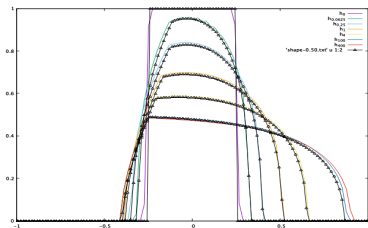
$Bi = 2$



$Bi = 1.25$



$Bi = 0.5$



## Two-viscosities model

$$\tau = \begin{cases} 2\mu_1 Dv & |Dv| \leq \frac{\tau^*}{2\mu_1} \quad \text{high viscosity} \\ 2\mu_2 Dv + \left(1 - \frac{\mu_2}{\mu_1}\right) \tau^* \frac{Dv}{|Dv|} & |Dv| > \frac{\tau^*}{2\mu_1} \quad \text{low viscosity} \end{cases}$$

$$\mu_2 = \mu_1$$

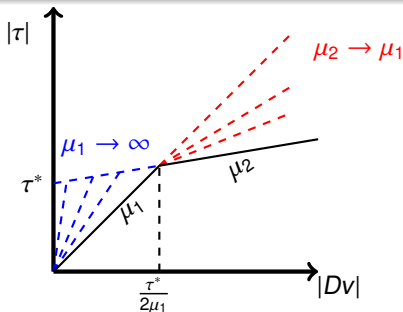
$$\mu_1 \rightarrow +\infty$$

$$\tau = 2\mu_1 Dv$$

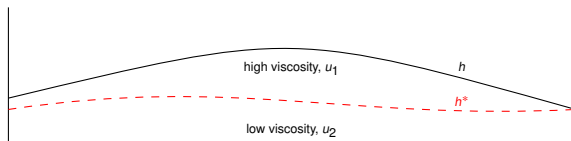
**Newtonian fluid**

$$\tau = \begin{cases} |\tau| < \tau^* & |Dv| \leq 0 \\ 2\mu_2 Dv + \tau^* \frac{Dv}{|Dv|} & |Dv| > 0 \end{cases}$$

**Bingham fluid**



# Two-viscosities model



## Difficulty

- 1 Induce unknown interface  $h^*$
- 2 Identify BC at interface  $h^*$

## Resolving

- 1 Choice of scaling + constraint on  $|Du|$
- 2 Preserve continuity of  $u$  and  $\tau$
- 3 Scale the viscosity:  $\mu_i = \alpha_i \mu$

## Two-viscosities model

$$\partial_t h - \partial_x \left( h_x \left( \frac{1}{\mu_2} \left[ \frac{h^{*3}}{3} - \frac{Y h^{*2}}{2} + Y h h^* - \frac{h h^{*2}}{2} \right] - \frac{1}{\mu_1} \left[ \frac{h^{*3} - h^3}{3} + h^2 h^* - h h^{*2} \right] \right) \right) = 0$$

$$Y = \max \left( h - \left( 1 - \frac{\mu_2}{\mu_1} \right) \frac{\sqrt{2} B}{|h_x|}, 0 \right), \quad h^* = \max \left( h - \frac{\sqrt{2} B}{|h_x|}, 0 \right)$$

$$\mu_2 = \mu_1$$

$$\partial_t h - \partial_x \left( \frac{h^3}{3} h_x \right) = 0$$

**Newtonian fluid**

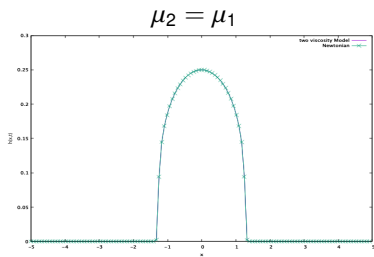
$$\mu_1 \rightarrow +\infty$$

$$h_t - \partial_x \left( \frac{h_x Y^2}{6} [3h - Y] \right) = 0$$

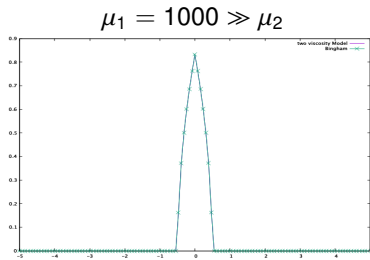
$$Y = \max \left( h - \frac{Bi \sqrt{2}}{|h_x|}, 0 \right)$$

**Bingham fluid**

# Numerical results



**Newtonian fluid**



**Bingham fluid**

# Slump test for two-viscosities fluid



**Thanks CEMRACS, 2019**

